Lecture 9

Chemical Reaction Engineering (CRE) is the field that studies the rates and mechanisms of chemical reactions and the design of the reactors in which they take place.

Lecture 9 – Thursday

Balances in terms of molar flow rates

- Block 1: **Mole Balances**

  Balance Equation on Every Species

- Block 2: **Rate Laws**

  Relative Rates

  Transport Laws

- Block 3: **Stoichiometry**
- Block 4: **Combine**

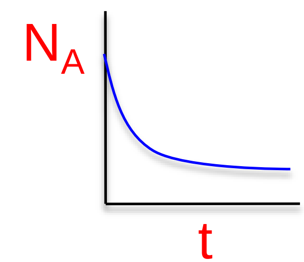
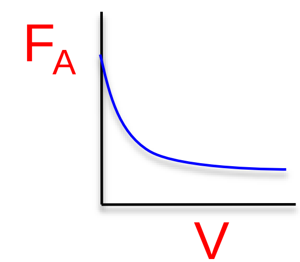
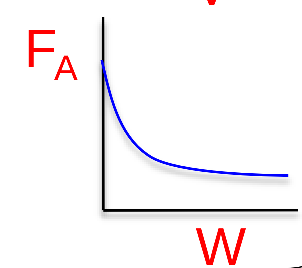
- **Membrane Reactors:**

Used for thermodynamically limited reactions

Review Lecture 1

Reactor Mole Balances Summary

The GMBE applied to the four major reactor types (and the general reaction A→B)

Reactor	Differential	Algebraic	Integral	
Batch	$\frac{dN_A}{dt} = r_A V$		$t = \int_{N_{A0}}^{N_A} \frac{dN_A}{r_A V}$	
CSTR		$V = \frac{F_{A0} - F_A}{-r_A}$		
PFR	$\frac{dF_A}{dV} = r_A$		$V = \int_{F_{A0}}^{F_A} \frac{dF_A}{dr_A}$	
PBR	$\frac{dF_A}{dW} = r'_A$		$W = \int_{F_{A0}}^{F_A} \frac{dF_A}{r'_A}$	

$$A + 2B \rightleftarrows C$$

Mole Balance

① Write mole balance on each species.†

$$\text{e.g., } \frac{dF_A}{dV} = r_A, \quad \frac{dF_B}{dV} = r_B, \quad \frac{dF_C}{dV} = r_C$$

↓

Rate Law

② Write rate law in terms of concentration.

$$\text{e.g., } -r_A = k_A\left(C_A C_B^2 - \frac{C_C}{K_C}\right)$$

↓

Relative Rates

③ Relate the rates of reaction of each species to one another.

$$\frac{-r_A}{1} = \frac{-r_B}{2} = \frac{r_C}{1}$$

$$\text{e.g., } r_B = 2r_A, \quad r_C = -r_A$$

↓

Stoichiometry

④ **(a)** Write the concentrations in terms of molar flow rates for isothermal ***gas-phase*** reactions.

$$\text{e.g., } C_A = C_{T0}\frac{F_A}{F_T}\frac{P}{P_0}, \quad C_B = C_{T0}\frac{F_B}{F_T}\frac{P}{P_0}$$

$$\text{with } F_T = F_A + F_B + F_C$$

(b) For ***liquid-phase*** reactions, use concentration, e.g., C_A, C_B

↓

Pressure Drop

⑤ Write the *gas-phase* pressure drop term in terms of molar flow rates.

$$\frac{dy}{dW} = -\frac{\alpha}{2y}\frac{F_T}{F_{T_0}}, \quad \text{with } y = \frac{P}{P_0}$$

↓

Combine

⑥ Use an ODE solver or a nonlinear equation solver (e.g., Polymath) to combine Steps ① through ⑤ to solve for, for example, the profiles of molar flow rates, concentration, and pressure.

† For PBR, use $\frac{dF_A}{dW} = r_A$, $\frac{dF_B}{dW} = r_B$, $\frac{dF_C}{dW} = r_C$.

Membrane Reactors

Membrane reactors can be used to achieve conversions greater than the original equilibrium value. These higher conversions are the result of ***Le Chatelier's principle***; you can remove the reaction products and drive the reaction to the right.

To accomplish this, a membrane that is permeable to that reaction product, but impermeable to all other species, is placed around the reacting mixture.

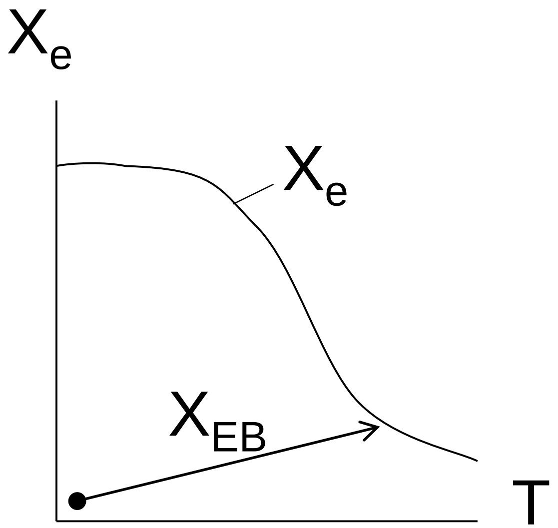
Membrane Reactors

<u>Dehydrogenation Reaction:</u>

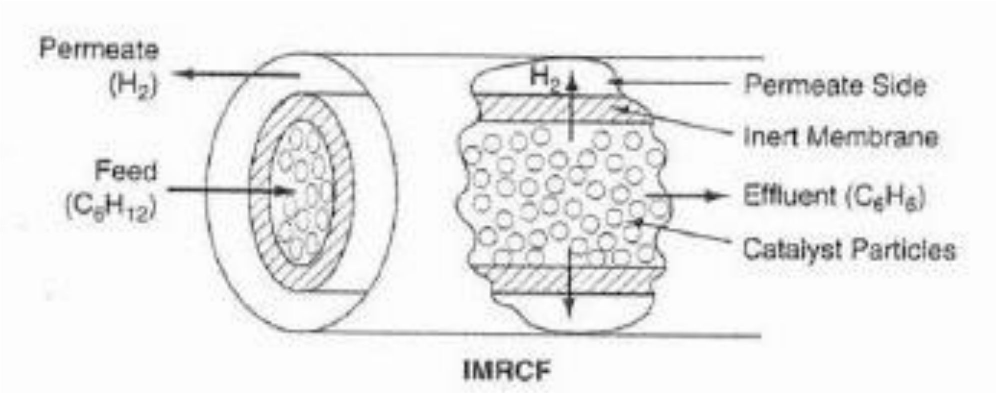
$C_3H_8 \leftrightarrow H_2 + C_3H_6$ $\qquad$ $A \leftrightarrow B + C$

<u>Thermodynamically Limited:</u>

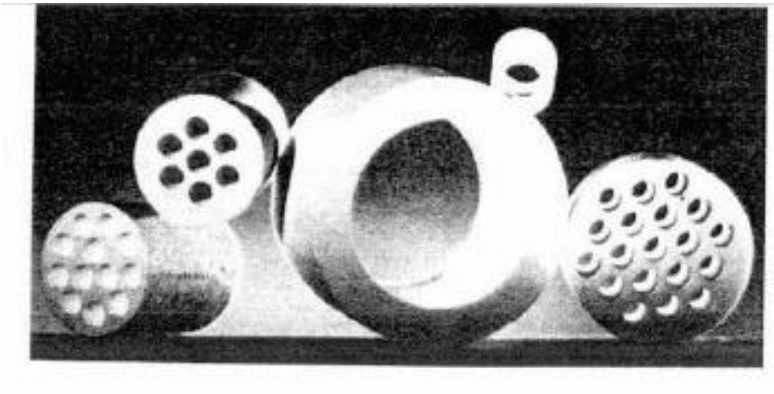
exothermic



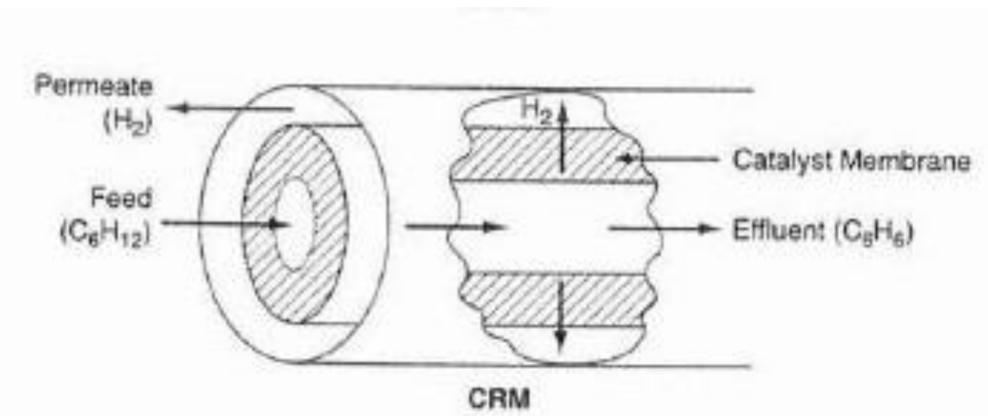
Membrane Reactors



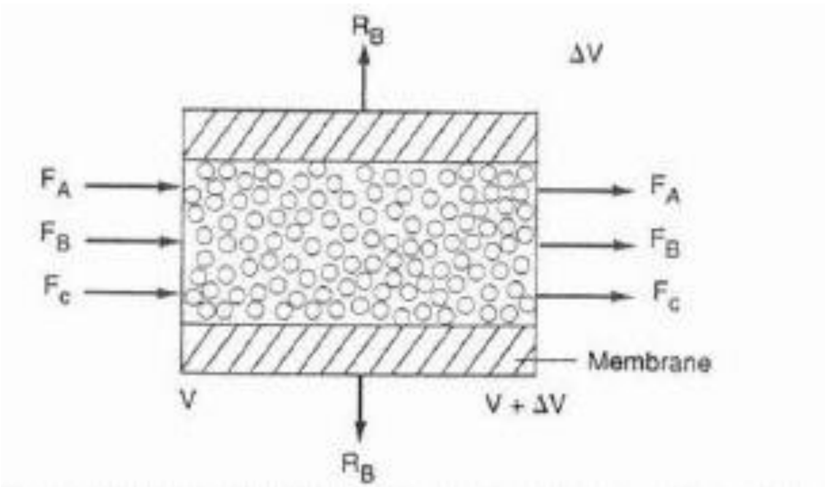
Cross section of IMRCF



Membrane Reactors

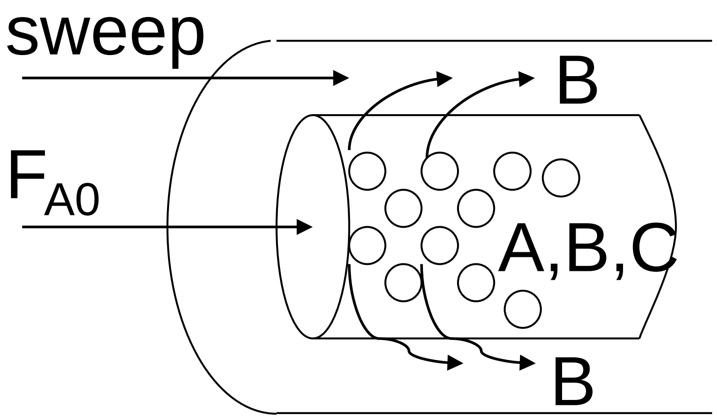


Cross section of CRM



Schematic of IMRCF for mole balance

Membrane Reactors

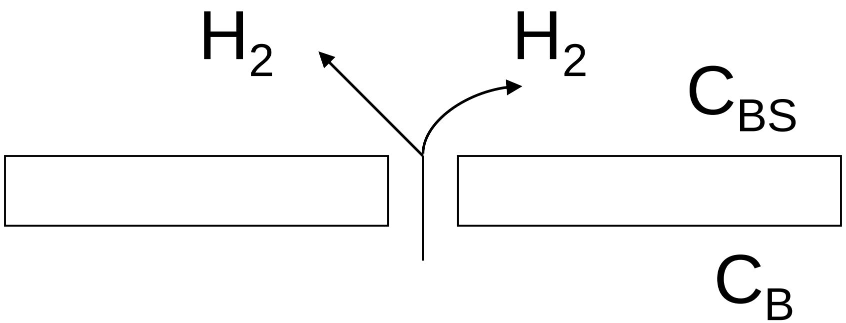


W = ρ_bV = solids weight

ρ_b = (1-ϕ)ρ_C= bulk solids density

ρ_C = density of solids

$$\rho_b = \frac{volume\ solids}{volume\ total} * \frac{mass\ of\ solids}{volume\ solids}$$



A,C stay behind since they are too big

Membrane Reactors

Mole Balance on Species A:

Species A: In – out + generation = 0

$$F_A\big|_V - F_A\big|_{V+\Delta V} + r_A \Delta V = 0$$

$$\boxed{\frac{dF_A}{dV} = r_A}$$

Membrane Reactors

Mole Balance on Species B:

Species B: In – out – out membrane + generation = 0

$$F_B\big|_V - F_B\big|_{V+\Delta V} - R_B \Delta V + r_B \Delta V = 0$$

$$\boxed{\frac{dF_B}{dV} = (r_B - R_B)}$$

$$R_B = \frac{\text{moles of B through sides}}{\text{volume of reactor}}$$

Membrane Reactors

$$W_B = k_C^{'}(C_B - C_{BS}) = \frac{\text{molar flow rate through membrane}}{\text{surface area of membrane}}\left[\frac{mol}{m^2 \cdot s}\right]$$

$$a = \frac{\text{membrane surface area}}{\text{reactor volume}} = \frac{\pi DL}{\frac{\pi D^2}{4}L} = \frac{4}{D} \quad \left[\frac{m^2}{m^3}\right]$$

$$R_B = W_B a = k_C^{'} a\left[C_B - C_{BS}\right]$$

$$k_C = k_C^{'} a$$

$$R_B = k_C\left[C_B - C_{BS}\right] \quad \left[\frac{mol}{m^3 \cdot s}\right]$$

Neglected most of the time

Membrane Reactors

Mole Balances:

$$(1) \quad \frac{dF_A}{dV} = r_A$$

$$(2) \quad \frac{dF_B}{dV} = r_B - R_B$$

$$(3) \quad \frac{dF_C}{dV} = r_C$$

Rate Law:

$$(4) \quad r_A = -k\left[C_A - \frac{C_B C_C}{K_C}\right]$$

Membrane Reactors

Relative Rates: $$\frac{-r_A}{1} = \frac{r_B}{1} = \frac{r_C}{1}$$

Net Rates: $$(5) \quad r_A = -r_B, \quad r_A = -r_C$$

Transport Law: $$(6) \quad R_B = k_C C_B$$

Stoichiometry: $$(7) \quad C_A = C_{T0}\frac{F_A}{F_T}$$ (isothermal, isobaric)

$$(8) \quad C_B = C_{T0}\frac{F_B}{F_T}$$

$$(9) \quad C_C = C_{T0}\frac{F_C}{F_T}$$

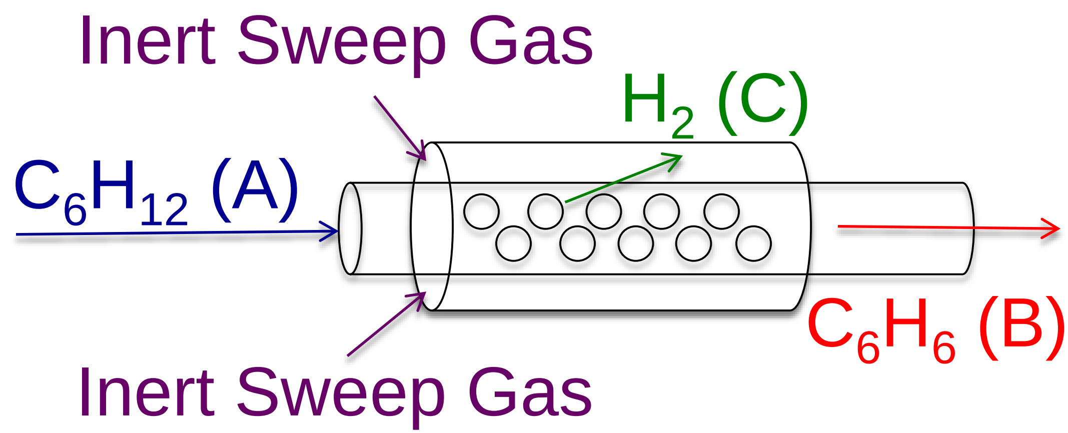
$$(10) \quad F_T = F_A + F_B + F_C$$

Parameters: $C_{TO} = 0.2, \; F_{A0} = 5, \; k = 4, \; K_C = 0.0004, k_C = 8$

Membrane Reactors

Example: The following reaction is to be carried out isothermally in a membrane reactor with no pressure drop. The membrane is permeable to product C, but impermeable to all other species.

$$C_6H_{12} \Leftrightarrow C_6H_6 + 3H_2$$
$$A \Leftrightarrow B + 3C$$



For membrane reactors, we cannot use conversion. We have to work in terms of the molar flow rates F_A, F_B, F_C.

Membrane Reactors

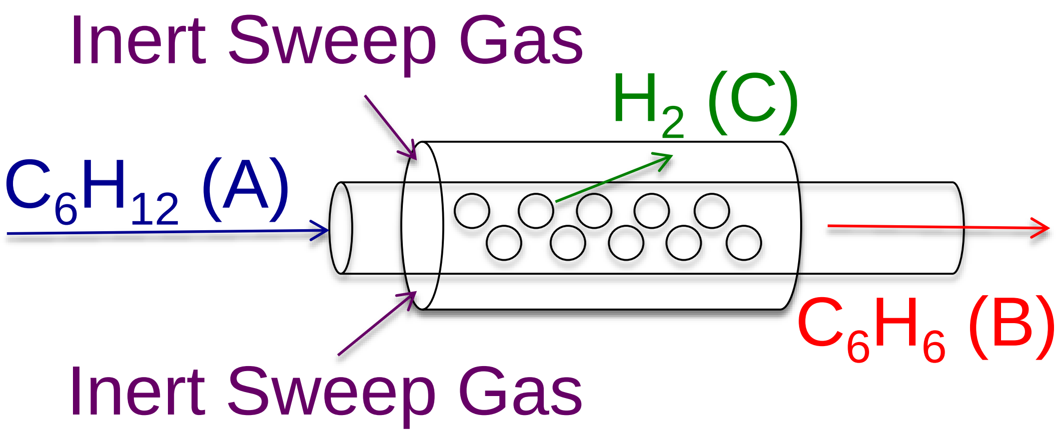
Mole Balances

$$C_6H_{12} \Leftrightarrow C_6H_6 + 3H_2$$
$$A \quad \Leftrightarrow B \quad + 3C$$

$$\frac{dF_A}{dW} = r_A'$$

$$\frac{dF_B}{dW} = r_B'$$

$$\frac{dF_C}{dW} = r_C' - k_C C_C$$



Membrane Reactors

Rate Law:

$$-r_A' = k_A\left[C_A - \frac{C_B C_C^3}{K_C}\right]$$

Relative Rates:

$$\frac{r_A'}{-1} = \frac{r_B'}{1} = \frac{r_C'}{3}$$

Net Rates:

$$r_B' = -r_A'$$

$$r_C' = -3r_A'$$

Membrane Reactors

Stoichiometry:

Isothermal, no Pressure Drop

$$C_{T0} = \frac{P_0}{RT_0}$$

$$C_A = C_{T0}\frac{F_A}{F_T}$$

$$C_B = C_{T0}\frac{F_B}{F_T}$$

$$C_C = C_{T0}\frac{F_C}{F_T}$$

$$F_T = F_A + F_B + F_C$$

Membrane Reactors

Combine: - Use Polymath

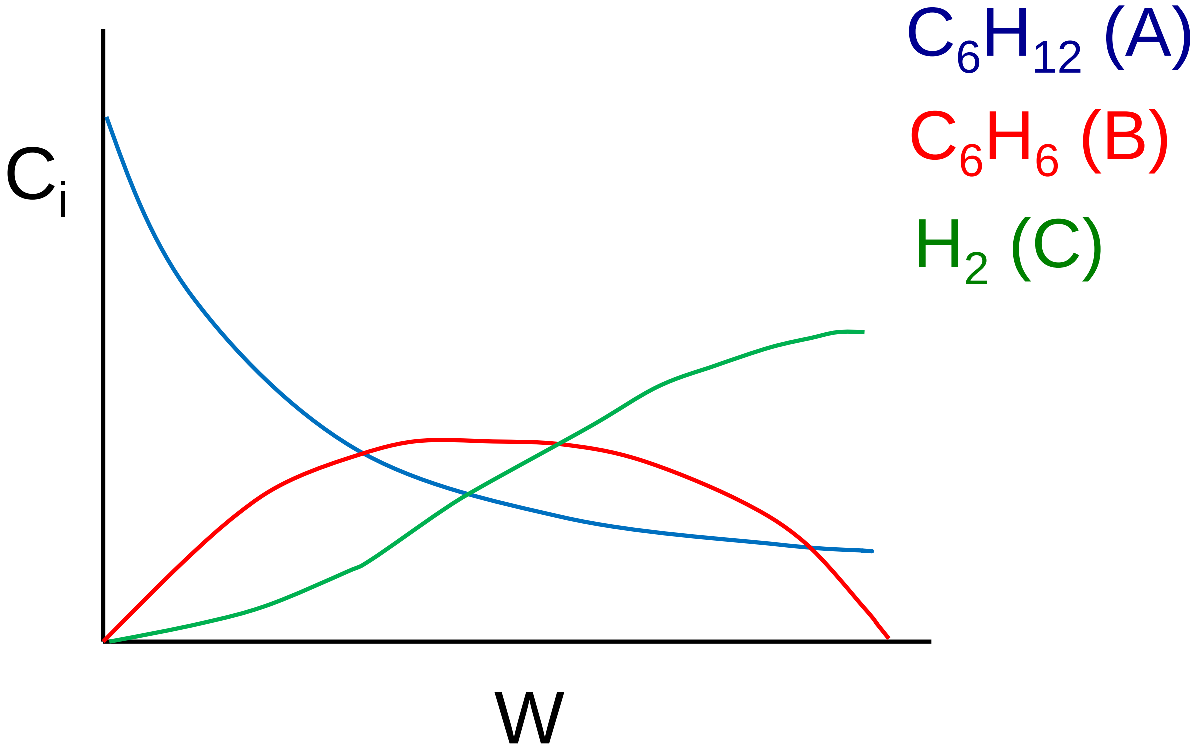
Parameters:

$$C_{T0} = 0.2 \frac{mol}{dm^3} \qquad F_{A0} = 10 \frac{mol}{s}$$

$$k_A = 10 \frac{dm^3}{kg\ cat\ s} \qquad k_C = 0.5 \frac{dm^3}{kg\ cat\ s}$$

$$K_C = 200 \frac{mol^2}{dm^6}$$

Membrane Reactors



End of Lecture 9